surface j by a straight-line route, and depends on size, orientation and spacing.





**View Factor:**  $F_{i \rightarrow i}$  is the fraction of diffuse radiation leaving surface i that arrives at







View factor is zero

View factor is one





















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$$F_{i \rightarrow j} = \frac{1}{A_{i}} \int_{A_{i}} \int_{A_{j}} \frac{\cos(\theta_{i}) \cos(\theta_{j}) dA_{i} dA_{j}}{\pi S^{2}}$$

$$A_{i} F_{i \rightarrow j} = A_{j} F_{j \rightarrow i}$$

$$F_{j \rightarrow i} = \frac{1}{A_{j}} \int_{A_{i}} \int_{A_{i}} \frac{\cos(\theta_{j}) \cos(\theta_{i}) dA_{j} dA_{i}}{\pi S^{2}}$$
Reciprocity relation





An **enclosure** is a three-dimensional region in space completely encased by bounding surfaces.





Openings (holes, cavities) that behave like a black body:



Read the text book about interior of rooms that appear black in day light, and the people that appear red-eyed in a picture.



# Example P.14-7

Two square plates of size 8 cm by 8 cm are directly opposite each other in parallel planes. What should the spacing between the plates be so that the view factor from one to the other is 0.5?





# Shape decomposition





# Radiative heat exchange between black bodies





# **Radiative heat exchange between diffuse and gray bodies**



Define radiocity as the sum of emitted and reflected radiation from a gray surface:

 $J = \varepsilon E_{b} + \rho G$   $\rho = 1 - \alpha$   $= 1 - \varepsilon$   $J = \varepsilon E_{b} + (1 - \varepsilon) G$   $J = E_{b} \text{ for a black surface}$ 



Net heat flux leaving surface i by radiation is the difference between outgoing and incoming radiation:

$$\frac{\mathsf{Q}_i}{\mathsf{A}_i} = \mathsf{J}_i - \mathsf{G}_i$$

Substitute for G<sub>i</sub>

For a gray, diffuse, isothermal surface:

$$\dot{\mathbf{Q}}_i = \frac{\mathbf{A}_i \ \varepsilon_i}{1 - \varepsilon_i} (\mathbf{E}_{bi} - \mathbf{J}_i)$$



$$\dot{\mathbf{Q}}_{1\rightarrow 2} = \mathbf{J}_1 \ \mathbf{A}_1 \ \mathbf{F}_{1\rightarrow 2} - \mathbf{J}_2 \ \mathbf{A}_2 \ \mathbf{F}_{2\rightarrow 1}$$
$$\dot{\mathbf{Q}}_{1\rightarrow 2} = \mathbf{A}_1 \ \mathbf{F}_{1\rightarrow 2} \ \left(\mathbf{J}_1 - \mathbf{J}_2\right)$$
$$\dot{\mathbf{Q}}_{2\rightarrow 1} = \mathbf{A}_2 \ \mathbf{F}_{2\rightarrow 1} \ \left(\mathbf{J}_2 - \mathbf{J}_1\right) = - \dot{\mathbf{Q}}_{1\rightarrow 2}$$
$$\dot{\mathbf{Q}}_i = \sum_{j=1}^N \dot{\mathbf{Q}}_{i\rightarrow j}$$



Electrical resistance analogy for an enclosure with gray, diffuse, isothermal surfaces



$$\hat{Q}_{i} = \frac{A_{i} \varepsilon_{i}}{1 - \varepsilon_{i}} (E_{bi} - J_{i})$$
$$= \frac{E_{bi} - J_{i}}{\frac{A_{i} \varepsilon_{i}}{1 - \varepsilon_{i}}} = \frac{E_{bi} - J_{i}}{R_{i}}$$

For a black surface  $R_i = 0$  and  $J_i = E_{bi}$ 

$$\dot{Q}_{1\to 2} = A_1 F_{1\to 2} (J_1 - J_2)$$
$$= \frac{J_1 - J_2}{A_1 F_{1\to 2}} = \frac{J_1 - J_2}{R_{1\to 2}}$$

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### **Two-surface enclosures**

# $R_{tot} = R_1 + R_{1 \rightarrow 2} + R_2$

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#### **ME – 212 THERMO-FLUIDS ENGINEERING II**

Large (infinite) parallel planes



$$\begin{array}{l} A_{1} = A_{2} = A \\ F_{1 \to 2} = 1 \end{array} \qquad \dot{O}_{1 \to 2} = \frac{A \sigma (T_{1}^{4} - T_{2}^{4})}{\frac{1}{\varepsilon_{1}} + \frac{1}{\varepsilon_{2}} - 1} \end{array}$$

Long (infinite) concentric cylinders



$$\frac{A_1}{A_2} = \frac{r_1}{r_2} \qquad \dot{O}_{1\to 2} = \frac{\sigma A_1 (T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{1 - \varepsilon_2}{\varepsilon_2} \left(\frac{r_1}{r_2}\right)}$$

$$\frac{A_1}{\varepsilon_1} = \frac{\sigma A_1 (T_1^4 - T_2^4)}{\frac{1}{\varepsilon_2} + \frac{1 - \varepsilon_2}{\varepsilon_2} \left(\frac{r_1}{r_2}\right)}$$

**Concentric spheres** 



$$\frac{A_{1}}{A_{2}} = \frac{r_{1}^{2}}{r_{2}^{2}} \qquad \dot{O}_{1 \to 2} = \frac{\sigma A_{1} (T_{1}^{4} - T_{2}^{4})}{\frac{1}{\varepsilon_{1}} + \frac{1 - \varepsilon_{2}}{\varepsilon_{2}} \left(\frac{r_{1}}{r_{2}}\right)}$$

Small convex object in large surroundings

$$A_1, T_1, \varepsilon_1$$

$$A_2, T_2, \varepsilon_2$$

$$\frac{A_1}{A_2} \approx 0$$
$$F_{1 \rightarrow 2} = 1$$

$$\dot{Q}_{1\to 2} = \sigma A_1 \varepsilon_1 (T_1^4 - T_2^4)$$

2



# Example P.14-23

A thermocouple is used to measure the temperature of a hot gas flowing in a pipe whose wall is at 350 C. A cylindrical radiation shield, large compared to the size of the thermocouple, encloses the thermocouple, as shown. The shield has an emissivity of 0.13. The emissivity of the thermocouple bead is 0.68 and the emissivity of the pipe wall is 0.94. The convective heat transfer coefficient on the thermocouple is 70 W/m<sup>2</sup>.K, and the thermocouple reads 500 C. The convective



heat transfer coefficient on the shield is 35 W/m<sup>2</sup>.K. The shield has a diameter of 6 cm. Calculate the actual gas temperature.

# Three-surface enclosures





There are 6 equations and 6 unknowns to be solved simultaneously





# Example P.14-30

A very long enclosure is formed from two perpendicular, equal-width plates and a slanted cover plate as shown. The cross section of the enclosure is in the shape of of an isosceles right triangle. Assuming gray and diffuse surfaces, calculate the net radiative heat transfer from the hottest plate.



